

Bailey 706 Safety Relief Valves

706 Safety Relief Valves

INTRODUCTION

The effects of exceeding safe pressure levels in an unprotected pressure vessel or system, can have catastrophic effects on both plant and personnel.

Safety relief valves should be used to protect any pressurised system from the effects of exceeding its design pressure limit.

A safety relief value is designed to automatically discharge gas, vapour or liquid from any pressure containing system, preventing a predetermined safe pressure being exceeded, and protecting plant and personnel.

Safety Valve

A valve which automatically discharges gases and vapours so as to prevent a predetermined safe pressure being exceeded. It is characterised by a rapid full opening action and is used for steam, gases or vapour service.

Relief Valve

A valve which automatically discharges fluid, usually liquid, when a predetermined upstream pressure is exceeded. The term is commonly used for pressure relieving valves in which the lift is proportional to the increase in pressure above the set pressure.

Safety Relief Valve

A valve which will automatically discharge gases, vapours or liquids, to prevent a predetermined safe pressure being exceeded. It is characterised by a rapid opening action.

DEFINITIONS

Set Pressure

The pressure measured at the valve inlet at which a safety relief valve should commence to lift under service conditions. **Overpressure**

The pressure increase above set pressure at the valve inlet at which the discharge capacity is attained. Usually expressed as a percentage of set pressure.

Accumulation

The pressure increase over a maximum safe working pressure of the vessel or system when the safety relief valve is discharging at its rated capacity is called accumulation. The term refers to the vessel or system to be protected and not to the valve. Accumulation is the same as over-pressure when the valve is set at the design pressure of the vessel.

Re-Seat Pressure

The pressure measured at the valve inlet at which the safety relief valve closes.

Blow-Down

The difference between the set pressure and the re-seating pressure expressed as a percentage of the set pressure or as a pressure difference.

Simmer

The pressure zone between the valve set pressure and the popping pressure. In this pressure zone the valve is only slightly open and therefore discharging a small percentage of its rated capacity.

Popping Pressure

The pressure at which the valve disc rapidly moves from a slightly open (simmer) position to a practically full open position.

Superimposed Back Pressure

Pressure higher than atmosphere in the safety relief valve outlet. This may result from discharge into the common disposal system of other safety relief valves or devices, or as a result of a specific design requirement. Back pressure can be either constant or variable depending on the operating conditions.

Built Up Back Pressure

The pressure existing at the outlet of a safety relief valve caused by flow through the valve into the disposal system.

Differential Set Pressure

This is the difference between the set pressure and the constant superimposed back pressure. It is applicable only when a conventional type safety relief valve is used to discharge against constant superimposed back pressure. (It is the pressure at which the safety valve is set at on the test bench without back pressure.)

Cold Differential Set Pressure

The pressure at which a safety relief valve, intended for high temperature service, is set on a test rig using a test fluid at ambient temperature. The cold differential test pressure will be higher than the set pressure, in order to compensate for the effect of elevated temperature on the valve.

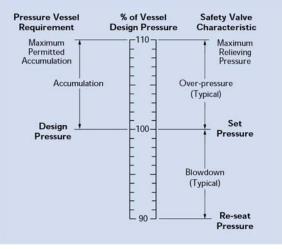
Valve Lift

The actual travel of the valve disc away from the seat when the valve is relieving.

Discharge Capacity

Actual rate of discharge of service media, which can be expressed in mass flow or volumetric terms.

PRESSURE TERM RELATIONSHIP



Note: System operating pressure must always be less than the re-seat pressure.

Equivalent Capacity

Calculated mass or volumetric flow rate of the valve of a given test fluid. The fluids commonly used for test purposes are steam, air and water.

SAFETY RELIEF VALV E – APPLICATIONS

Application	Medium	Safety Relief Valve Type
Vented boilers	Hot Water	706
Un-vented boilers		716
		746/766
		Рор
		716T
Boiler, pipeline and	Steam	706/716
vessel protection		746
		756/766
		Рор
		1640B
		300
Compressor pipeline	Air	706
and receiver protection		716
		746
		POP
		1640B
		300
Pipeline and vessel	Cold Water	706
protection		716
		746
		1640B
		300
Pump Protection	Liquids	480/485
Process pipeline, pump	Process/Corrosive Liquids	716 Stainless steel
and vessel protection		746 Stainless steel
		490 Stainless steel
Clean steam and	Steam and Gases	716 Stainless steel
nygienic environments		746 Stainless steel
Pipework, tank and	Cryogenic Gases	776
equipment protection		
Pipework, tank and	Cold & Fine Gases	716
equipment protection		776
Blowers, bulk transfer,	Air	616D
ank duty, road/rail transfers		

Pressure - capacity - material - temperature - fluid - connection required.

706 Safety Relief Valve



TECHNICAL SPECIFICATION

Approvals

BS6759 Pt 1, 2, & 3 PED certified Category IV Water Regulation Advisory Scheme (WRAS)

Materials

- Body Bronze to 220°C
- Trim Viton to 200°C
 - Brass to 220°C
 - EPDM for potable water to 95°C

Note: The brass disc (not soft discs) should be used on all steam applications

Maximum Back Pressure

Barg 5.5 Constant 80% 10% Built-up Variable 0% (Total % must not exceed Barg shown) **Connections** Screwed In x Screwed Out Flanged In x Screwed Out Construction Top Guided / High Lift **Cap Options** Open lever Pressure tight dome Sizing Refer to Capacity Charts

	Orifice	Min (Barg)	Max (Barg)
Size	mm²	Pressure	Pressure
DN15 (1/2")	126	0.35	12.5
DN20 (3/4")	364	0.35	12.5
DN25 (1")	481	0.35	12.5
DN32 (1-1/4")	791	0.35	12.5
DN40 (1-1/2")	1240	0.35	12.5
DN50 (2")	1943	0.35	12.5

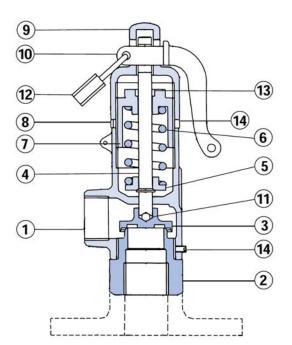
		Over	Blow
	Kdr	pressure	down
Steam	0.173	10%	15%*
Hot water	0.173	10%	15%*
Air / Gas	0.173	10%	10%*
Liquid	0.149	10%	20%+

DESIGN

The 706 Safety Relief Valve is designed to take full advantage of its high lift capability by incorporating top guiding, which provides an unobstructed seat bore.

Positive re-seating is achieved by a freely pivoting disc in the standard valve. The Viton trim is suitable for air, gas, vapour, or liquid duties up to 200°C providing good resistance to chemical attack. The metal disc option is primarily designed for use on steam duties and high temperature duties above 200°C. An EPDM disc is also available for potable water duties up to 95°C.

Test levers are available for inline safety checking, alternatively a sealed dome can be supplied for service conditions requiring a pressure tight seal on the discharge side, eg. liquid service with enclosed discharge.



ITEM	PART	MATERIAL
1	Body	Bronze
2	Seat	Bronze
3*	Disc	Various
4	Spindle	Brass
5	Spring Cap	Brass
6*	Spring	Chrome vanadium
7	Adjusting Screw	Bronze
8	Locking Ring	Bronze
9+	Dome	Nylon
10	Lever	Bronze
11*	Ball	Stainless Steel
12	Padlock	Brass
13	Bush	PTFE
14	Pinning Screw	Steel
Note:		

* Recommended spares.

+ Synthetic dome should not be adjacent to external heat sources.

Flange options: BS10 Table E and F, BS4504 PN16/25 and ANSI 150.

DIMENSIONS

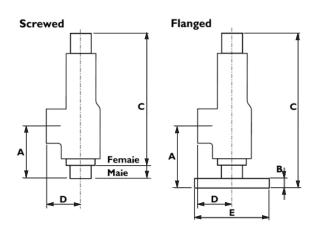


FIGURE NUMBERING

706					
TRIM	CONNECTIO	NS	CAP		
E EPDM V Viton M Metal	S Screwed in and out (Inlet available Male or Female)		D Pressure tight dome		
	F Flanged in screwed out		L Open lever		

Valve	Valve	Inlet	Outlet		'C' '	C'		Weight		
Туре	Size			Α	Dome	Lever	D	(kg)		
	DN15	1/2"	1/2"	48	129	151	29	1.0		
lale	DN20	3/4"	3/4"	56	159	181	37	1.6		
Fen	DN25	1"	1"	78	185	208	40	2.0		
ex	DN32	1-1/4"	1-1/4"	90	205	238	48	3.5		
Male x Female	DN40	1-1/2"	1-1/2"	93	241	274	56	5.0		
_	DN50	2"	2"	110	299	334	71	7.0		
e	DN15	1/2"	1/2"	40	111	133	29	0.6		
ma	DN20	3/4"	3/4"	46	140	162	37	1.0		
Female x Female	DN25	1"	1"	56	163	186	40	1.5		
ale	DN32	1-1/4"	1-1/4"	67	182	215	48	3.0		
e	DN40	1-1/2"	1-1/2"	67	216	249	56	4.5		
ш.	DN50	2"	2"	79	268	303	71	6.0		
Valve	Valve	Inlet	Outlet			'C'	"C"			Weight
Туре	Size			Α	В	Dome	Lever	D	Е	(kg)
ale	DN20	3/4"	3/4"	70	10	164	186	37	114	1.9
eme	DN25	1"	1"	71	11	179	202	40	121	2.6
Т Т	DN32	1-1/4"	1-1/4"	90	12.7	206	239	48	140	4.7
ged	DN40	1-1/2"	1-1/2"	94	12.7	243	276	56	150	6.5
Flanged x Female	DN50	2"	2"	110	12.7	298	333	71	165	8.5

AIR CAPACITY CHART (I/s) @ 0.3 Barg or 10% overpressure* and 15°C

Set Pressure (Barg)		2	Valve Ty (BS6759	pe 706) Pt2)		
	DN15	DN20	DN25	DN32	DN40	DN50
0.35	5.03	14.5	19.2	31.5	49.5	77.5
1.0	8.97	25.9	34.2	56.3	88.3	138
2.0	13.9	40.0	52.9	87.0	136	214
3.0	18.1	52.4	69.2	114	178	280
4.0	22.8	65.8	86.9	143	224	351
5.0	27.3	79.1	105	172	270	422
6.0	32.0	92.5	122	201	315	493
7.0	36.6	106	140	230	361	565
8.0	41.3	119	158	259	406	636
9.0	45.9	133	175	288	452	708
10.0	50.5	146	193	317	497	779
12.0	59.8	173	228	375	588	921
12.5	62.1	179	237	390	611	957
14.0						
16.0						
18.0						
20.0						
22.0						
24.0						
26.0						
28.0						
30.0						
32.0						
34.0						
36.0						
38.0						
40.0						

* Minimum overpressure = 0.07 Barg at set pressure less than 1.0 Barg.

Useful Conversions

 $Nm^{3}/h = 1/sec \times 3.60$ SCFM = 1/sec x 2.12

Other Gases

If you wish to use the valve on other compatible gases, the sizing details above can be used. The valve capacity will however change depending on the specific gravity of the flowing gas. Multiply the valve air capacity by $1/\sqrt{SG}$ to give the gas capacity. SG = specific gravity (relative to air = 1).

SATURATED STEAM CAPACITY CHART (kg/h)

Set Pressure (Barg)	Saturated Steam Temp. °C	(B	S6759 P	Valve T t1 @ 10	ype 706)% Over	; pressur	e)*
		DN15	DN20	DN25	DN32	DN40	DN50
0.35	108	11.1	32.0	42.3	69.5	109	171
1.0	120	22.3	64.4	85.1	140	219	344
2.0	134	36.6	106	140	230	360	564
3.0	144	49.4	143	188	310	486	761
4.0	152	62.0	179	237	389	610	955
5.0	159	74.5	215	285	468	734	1150
6.0	165	87.1	252	333	547	857	1344
7.0	170	99.7	288	381	626	981	1538
8.0	175	112	324	429	705	1105	1732
9.0	180	125	361	477	784	1229	1926
10.0	184	138	397	525	863	1353	2120
12.0	192	163	470	621	1021	1601	2508
12.5	193	169	488	645	1061	1663	2605
14.0	198						
16.0	204						
18.0	210						
20.0	215						
22.0	220						
24.0	224						
26.0	228						
28.0	232						
30.0	236						
32.0	239						
34.0	243						
36.0	246						
38.0	249						
40.0	252						

* Minimum overpressure = 0.07 Barg at set pressure less than 0.7 Barg. Minimum overpressure = 0.07 Barg at set pressure less than 1.0 Barg.

Useful Conversions

 $lbs/h = kg/h \times 2.2046$

Other Temperatures

The steam tables on these pages are based on saturated steam, at the temperatures shown. For steam systems operating at higher temperatures, the above capacities will need to be derated by using the super heat correction factor.

WATER CAPACITY CHART (I/min) @ 10% overpressure* @ 20°C

Set Pressure (Barg)			Valve Ty (BS6759	pe 706) Pt3)		
	DN15	DN20	DN25	DN32	DN40	DN50
0.35	10.3	29.8	39.4	64.8	102	159
1.0	16.7	48.3	63.8	105	164	258
2.0	23.6	68.3	90.2	148	233	364
3.0	28.9	83.6	111	182	286	446
4.0	33.4	96.5	128	210	329	515
5.0	37.4	108	143	235	368	576
6.0	40.9	118	156	257	403	631
7.0	44.2	128	169	278	435	682
8.0	47.3	137	180	297	465	729
9.0	50.1	145	191	315	493	773
10.0	52.8	153	202	332	520	815
12.0	57.9	167	221	363	570	893
12.5	59.1	171	226	371	581	911
14.0						
16.0						
18.0						
20.0						
22.0						
24.0						
26.0						
28.0						
30.0						
32.0						
34.0						
36.0						
38.0						
40.0						

*Minimum overpressure = 0.07 Barg at set pressure less than 0.7 Barg.

Useful Conversions

 $Igpm = 1/min \ge 0.22$ m³/min = 1/min \ge 0.001

Other Liquids

If you wish to use the valve on other compatible liquids, the sizing details above can be used. The valve capacity will however change depending on the specific gravity of the flowing liquid. Multiply the valve water capacity by 1/SG to give the liquid capacity. SG = specific gravity (relative to water = 1).

HOT WATER CAPACITY CHART (kW) FOR A PRESSURISED (un-vented) SYSTEM

Set Pressure (Barg)	(Valve Type 706 (BS6759 Pt1 @ 10% Overpressure)*								
	DN15	DN20	DN25	DN32	DN40	DN50				
0.35	14.3	41.4	54.7	89.9	141	221				
1.0	16.4	47.5	62.8	103	162	254				
2.0	23.1	66.9	88.4	145	228	357				
3.0	30.9	89.4	118	194	304	477				
4.0	38.8	112	148	244	382	599				
5.0	46.7	135	178	293	460	720				
6.0	54.6	158	208	343	537	842				
7.0	62.5	181	239	392	615	964				
8.0	70.5	203	269	442	693	1085				
9.0	78.3	226	299	491	770	1207				
10.0	86.2	249	329	541	848	1329				
12.0	102	294	389	640	1003	1572				
12.5	106	306	404	665	1042	1633				
14.0										
16.0										
18.0										
20.0										
22.0										
24.0										
26.0										
28.0										
30.0										
32.0										
34.0										
36.0										
38.0										
40.0										

* Minimum overpressure = 0.07 Barg at set pressure less than 0.7 Barg. Minimum overpressure = 0.07 Barg at set pressure less than 1.0 Barg.

NOTE:

Pressurised (un-vented) hot water systems have the entire discharge capacity handled solely by the valve. **Open vented systems** take into account the discharge capacities of the vent. Hence the equivalent discharge of the valve/system is considered to be double the above chart capacities.

INSTALLATION

Safety Relief Valves should always be installed in an upright position with their spring chamber vertical.

All packing materials should be removed from the valve connections prior to installation.

Pressure Vessels

When fitting a Safety Relief Valve onto pressure vessels, the inlet connection pipe should be as short as possible and the bore should be at least equivalent to the nominal bore size of the valve.

The pressure drop between the vessel and the valve should be no more than 3% at rated capacity.

A pressure-tight dome should be specified when:

1) A back pressure must be contained within the relieving system.

2) A head of liquid is built up within the valve body and consequently needs to be contained.

3) The relieving medium is toxic, corrosive or environmentally unfriendly.

Pipelines

When fitting a Safety Relief Valve into a pipeline, the inlet connecting pipe leading from the main pipeline to the Safety Relief Valve should be as short as possible, so that the inlet pressure drop is no more than 3% of rated capacity. In addition, it is advised that the Safety Relief Valve is placed a sufficient distance downstream of the pressure source. This will protect the valve from the adverse effects of pressure pulsations.

Discharge Pipelines

These should be equal to or larger than the valve outlet, with adequate supports, minimum number of bends and overall length. Unless balanced bellows valves are installed, the maximum built up backpressure should not exceed 10% of the set pressure, although the 746, 756 and the 766 can handle higher back pressure if required. Steam service valves should be adequately drained.

Alignment of the discharge or drain should present no risk to persons or property. Protection from the collection of rainwater or condensation in the discharge pipe is advisable.

System Cleansing

It is essential that new installations are fully flushed and all debris removed prior to installing the valve as serious damage can be caused to valve seats, resulting in subsequent leakage.

Pressure Adjustment

Every valve is fitted with a suitable spring and tested before leaving the factory. Valves can be preset on request but to alter the set pressure, the adjusting screw, when viewed from the top, should be screwed downwards in a clockwise direction to increase the set pressure and upwards in an anti-clockwise direction to decrease it. Set pressure adjustment must be carried out by experienced and approved personnel. Any change in set pressure must be within the range of the existing spring, if it exceeds the range, a new spring will be required. The cap lead seal must be re-made after any adjustment to the set pressure.

Blow-down Adjustment (POP, 756 & 766 valves only)

The blow-down ring (part no. 8) is set before the valve leaves the factory and normally no further adjustment will be necessary. However, if the reseating pressure has to be altered in service, the blow-down ring should be screwed (downwards) clockwise to raise the re-seat, popping and simmer pressures. If the blowdown ring is screwed (upwards) anti-clockwise the re-seat, popping and simmer pressures will lower. When re-inserting the setting screw (part no 9.) it should always be placed to engage a slot in the blow-down ring. The standard blowdown is 5% for 756, 10% for 766 and 10% for a POP type valve (minimum 0.3 Barg for all three valve types).

For recommended settings, please contact our technical sales office who will be pleased to help.

COLD DIFFERENTIAL TEST PRESSURE

When setting a valve intended for use at high temperature on a test rig using a test fluid at ambient temperatures, it is necessary to set the valve at a slightly higher pressure, so that it will open at the correct set pressure under operating conditions. The necessary allowance is shown in the following table.

Operating temperature	Increase in set pressure at ambient temperature
Up to 121°C	None
122°C to 316°C	1%
317°C to 427°C	2%

706 SPRING SELECTION CHARTS

DN15 Spri	ing Range			DN32 Spr	ring Range		
Part No	Barg	Psig	Colour code	Part No	Barg	Psig	Colour code
C2193	0.35 – 1.0	5 – 15	Red	C2220	0.35 – 1.0	5 – 15	Red
C2194	1.0 – 1.7	15 – 25	Blue	C0174	1.0 – 1.7	15 – 25	Blue
C2195	1.7 – 2.4	25 – 35	Orange	C2213	1.7 – 2.4	25 – 35	Orange
C2196	2.4 – 3.5	35 – 50	Orange/Blue	C2221	2.4 – 4.1	35 – 60	Orange/Blue
C2197	3.5 – 5.5	50 - 80	Green/White	C2214	4.1 – 5.5	60 – 80	Purple
C2198	5.5 – 8.3	80 – 120	Green/Blue	C2222	5.5 – 8.3	80 – 120	Green/White
C2199	8.3 – 12.5	120 – 180	White/Blue	C2215	8.3 – 10.3	120 – 150	Green/Blue
				C2223	10.3 – 12.5	150 – 180	White/Blue

DN20 Spring Rang

Part No	Barg	Psig	Colour code	DN40 Spring Rang			
C2187	0.35 – 1.0	5 – 15	Red	Part No	Barg	Psig	Colour code
C2188	1.0 – 1.7	15 – 25	Blue	C2224	0.35 – 1.0	5 – 15	Red
C2189	1.7 – 3.5	25 – 50	Orange	C2216	1.0 – 1.7	15 – 25	Blue
C2190	3.5 – 6.9	50 – 100	Orange/Blue	C0709	1.7 – 2.4	25 – 35	Orange
C2191	6.9 – 10.3	100 – 150	Purple	C2225	2.4 – 4.1	35 – 60	Orange/Blue
C2192*	10.3 – 12.5	150 – 180	Green/White	C2226	4.1 – 5.5	60 – 80	Purple
C2200†	10.3 – 12.5	150 – 180	White/Blue	C2217	5.5 – 8.3	80 – 120	Green/White
·				C2208	8.3 – 10.3	120 – 150	Green/Blue
* For air or steam				C2218	10.3 – 12.5	150 – 180	White/Blue

* For air or steam

+ For water or liquids

DN25 Spring Range

•	ning Kange			Part No	Barg	Psig	Colour code	
Part No	Barg	Psig	Colour code	C2227	0.35 – 1.0	5 – 15	Red	
C0139	0.35 – 1.0	5 – 15	Red					
C0145	1.0 – 1.7	15 – 25	Blue	C0718	1.0 – 1.7	15 – 25	Blue	
C0147	1.7 – 2.4	25 – 35	Orange	C0719	1.7 – 2.4	25 – 35	Orange	
			U U	C2219	2.4 – 4.1	35 – 60	Orange/Blue	
C2182	2.4 – 4.1	35 – 60	Orange/Blue	C2228	4.1 – 5.5	60 – 80	Purple	
Air and Pumped Liquids only				C2229	5.5 – 8.3	80 – 120	Green/White	
C2183	4.1 – 5.5	60 – 80	Purple					
C2184	5.5 – 8.3	80 – 120	Green/White	C2209	8.3 – 10.3	120 – 150	Green/Blue	
C2185	8.3 – 10.3	120 – 150	Green/Blue	C2230	10.3 – 12.5	150 – 180	White/Blue	
C2186	10.3 – 12.5	150 – 180	White/Blue					
Steam and Hot Water only								
C2183	4.1 – 6.9	60 – 100	Purple					
C2184	6.9 – 10.3	100 – 150	Green/White					
C2185	10.3 – 12.5	150 – 180	Green/Blue					

DN50 Spring Range

Springs listed above comply with the requirements of BS6759: Part 1.

700 SERIES TECHNICAL SPECIFICATION

Fig. No	706	716	746	756	766	776
Body	Bronze	Bronze	Cast Steel	Cast Iron	Cast Steel	Bronze
Material		Cast Iron	Stainless Steel		Cast Steel	
		Stainless Steel				
Code		BS6759				ADMERKBLATT
Approvals Part	1, 2, & 3	1, 2, & 3	1, 2, & 3#	1	1	A2
Top Guided	Yes	Yes	Yes	Yes	Yes	Yes
Lift	High Lift	Full Lift	Full Lift	Full Lift	High Lift	Full Lift
	DN15-50	DN15-50	DN25-100	DN25-80	DN40-80	DN15-50
Size Range	1/2" – 2"	1/2" – 2"	1" – 4"	1" – 3"	1-1/2" – 3"	1/2" – 2"
Orifice Areas						
(mm2)						
DN15	126	109	_	—	—	
DN20	364	314	_		_	
DN25	481	415	415	415	_	Sizing data
DN32	791	660	660	660	_	to TUV
DN40	1240	1075	1075	1075	2280	available
DN50	1943	1662	1662	1662	4054	on request.
DN65	_		2827	2827	6334	•
DN80	_	_	4301	4301	9121	
DN100	_	_	6648	_	_	
Pressure Range†						
(Barg)	0.35 to 12.5	0.35 to 32	0.35 to 40	0.35 to 24	0.35 to 24	1 to 41.3
Temp Range (°C)						
(with suitable material)	-59 to +220	–90 to +260	-40 to +427	–29 to +300	–29 to +230	-196 to +60
Connection	Screwed	Screwed	Flanged	Flanged	Flanged	Screwed
	Flanged	Flanged				
Trim Options	Brass	Stainless	Stainless	Stainless	Stainless	KEL F
	EPDM (WRC)	Aflas	Aflas	EPDM	EPDM	(PCTFE)
	Viton	EPDM	EPDM			
Cap Options	Dome	Dome	Dome	Open lever	Open lever	Dome
	Open lever	Open lever	Open lever			
			Packed lever			
Kdr. Cert. Coeff.						
Steam/Hot Water/Gases	0.173	0.7	0.7	0.716	0.4	
Kdr. Cert. Coeff.						
Liquids	0.149	0.46	0.46		_	
Pressure	Brz 5.5 Barg	SS 5.5 Barg	SS 16 Barg	CS 12 Barg	CS 12 Barg	SS 5.5 Barg
Maximum Constant	80%	80%	80%		_	80%
Back Built-up	10%	10%	10%	50%	50%	10%
Pressure* Variable	_	_	40%			

*For higher back pressures consult factory. **Resilient 766 is limited to 10%.

†For maximum pressure per size and material refer to capacity and spring charts, pages 14 to 23. ††716 EPDM Seat, max pressure of 12.5 Barg on DN 15, 20, 25 and 18 Barg on DN 32, 40, 50. #746 is also available ASME VIII and AD Merkblatt A2 certified, details available on request.

Material	Seat		Body	
Temperature	EPDM (WRC)	-40 °C to 95 °C	Bronze BSI 400 - LG2	-196 c to 232 °C
Limitations	EPDM	-50 °C to 150 °C	Cast Iron BSI 452-260	-10 C to 300 °C
	Aflas	-10 °C to 200 °C	Carbon Steel SA216-WCB	-29 C to 427 °C
	Brass	-59 °C to 232 °C	Stainless Steel 316/CF8M	-90 C to 427 °C
	Stainless Steel	-90 °C to 232 °C		